# The Specific Catalytic Activity of Sodium Faujasites in H<sub>2</sub>S Oxidation

Z. DUDZIK<sup>1</sup> AND M. ZIÓLEK

Institute of Chemistry, A. Mickiewicz University, 60-780 Poznań, Poland

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The H<sub>2</sub>S oxidation reaction with molecular oxygen on sodium faujasites was investigated in a flow system within the temperature range 0-300°C and using ESR and UV methods. Elemental sulfur is the primary product, but at temperatures above 20°C substantial amounts of SO<sub>2</sub> were observed in the reaction products. At higher temperatures (70-300°C) NaY is distinctly more active than NaX. The specific high catalytic of sodium faujasites in the H<sub>2</sub>S oxidation reaction was observed. This activity is due to the generation of the zeolite surface of radicals such as  $\cdot S_x \cdot$ , HS<sub>x</sub> $\cdot$ , O<sub>2</sub> $\cdot$ <sup>-</sup>, SO<sub>2</sub> $\cdot$ <sup>-</sup>, SO<sub>3</sub> $\cdot$ <sup>-</sup>, and H<sub>2</sub>S<sub>2</sub> $\cdot$ <sup>-</sup>. These species take part in the reaction as intermediate compounds, and their concentrations strongly influence the reaction rate. On the basis of the results of kinetic and catalytic experiments and literature data, hypotheses concerning some initial reaction steps are presented and discussed.

## INTRODUCTION

The reaction of hydrogen sulfide and oxygen to form elemental sulfur and water is known to respond to many different catalysts. The most common catalysts are silica gels, silicates (mainly Fe), activated carbon, alkali and alkaline earth metals, oxides and sulfides, and especially catalysts derived from aluminum oxide or natural bauxite (1, 2).

The oxidation reaction of  $H_2S$  on these catalysts in a dynamic system proceeds at relatively high temperatures, mainly within the range of 250-400°C. Using a static system and special reaction conditions (efficient outgassing of the samples, low or relatively low pressures of  $H_2S$ ), Deo *et al.* (3) observed the oxidation of  $H_2S$  at room temperature on  $\gamma$ -alumina and zeolite NaY, and Slager and Amberg (4) made similar studies on  $\eta$ - and  $\gamma$ -alumina. Kerr

<sup>1</sup> Address reprint requests to Z. Dudzik, Alberta Research Council, 11315-87th Avenue, Edmonton, Alberta, T6G 2C2 Canada. and Johnson (5), while passing gaseous hydrogen sulfide over a powdered 13X molecular sieve in air at room temperature. observed free sulfur deposited on the catalyst surface. One of us (6) investigated the oxidation of  $H_2S$  to elemental sulfur in a static system on NaX (Linde  $13\times$ ) zeolite and observed that this reaction occurs even at  $-80^{\circ}$ C. Immediately after admission of  $O_2$  at  $-80^{\circ}C$  to activated NaX zeolite containing H<sub>2</sub>S adsorbed at room temperature, the sample became strongly paramagnetic and the ESR spectrum showed the presence of sulfur biradicals  $\cdot S_{-}(S)_{x}$ -S. The sulfur-, oxygen-, and sulfur-oxygen radicals taking part in the H<sub>2</sub>S oxidation reaction as intermediate compounds have been identified and described in earlier papers (7, 8).

The mechanism of the catalytic oxidation of  $H_2S$  was investigated also by Steijns *et al.* (9-11). These authors concluded that the catalytically active phase in this process is liquid sulfur which may be deposited on different matrices. They proposed a redox model for this process in which the reaction between oxygen molecules and deposited sulfur is the oxidation stage, and the reaction between dissociatively adsorbed  $H_2S$ and chemisorbed oxygen is the reduction stage.

The aim of this paper is to synthesize the former (7, 8) and the new results and to present on the basis of ESR and catalytic experiments some proposals concerning the initial steps of the H<sub>2</sub>S oxidation reaction with molecular oxygen on sodium faujasites.

# EXPERIMENTAL

The continuous flow technique was used for the measurements of catalytic activity. The U-shaped Pyrex glass reactor (i.d., 12 mm; total volume, 24 ml) fitted with Teflon stopcocks and containing 1.1 g of zeolite in dehydrated form was mounted in an ultrathermostat (for experiments carried out in the temperature range 0-200°C) or in an electric furnace (200-300°C). A 37-ml/min gas flow containing 2.7% vol of H<sub>2</sub>S and different amounts of  $O_2$  and  $N_2$  passed through the reactor to a gas chromatographic assembly. The  $O_2$ :  $H_2S$ ratio was 1:1, or 7.5:1. A 70-cm glass column (i.d., 4 mm) containing Porapak Q. 120-150 mesh at 80°C, served to separate the products (carrier gas,  $N_2$ ; 40 ml/min), which were subsequently detected and measured by a flame photometric detector (Jeol JGC-1100 FPD) and amplifier. H<sub>2</sub>S was Fluka research grade. NaX was Linde 13X Lot No. 1360027 and NaY was Linde SK-40 Lot No. 3606411, both supplied in powder form. In the ESR experiments the zeolites were used in powder form, activated under a 10<sup>-4</sup>-Torr vacuum at 350°C for 3 hr. In the kinetic experiments the zeolite crystallites were tableted under pressure, ground, sieved to the 1- to 1.5-mm diameter range and activated in flowing helium at 350°C for 4 hr.

The ESR spectra were obtained with a Varian T-line spectrometer and accessories,

and uv spectra with a Unicam SP-700 spectrometer.

#### RESULTS

Hydrogen sulfide was oxidized at 70 and 300°C with molecular oxygen on NaX zeolite and on sodium silica-alumina obtained from the full collapse of the zeolite structure after 12 hr of heating of the NaX zeolite at 920°C. The  $O_2: H_2S$  ratio was 7.5:1. Results presented in Fig. 1 indicate the strong influence of the faujasite structure on this reaction when conducted at 70°C.

The H<sub>2</sub>S oxidation reaction on NaX and NaY zeolites was carried out at an O<sub>2</sub>: H<sub>2</sub>S ratio of 7.5:1 at temperatures 0, 20, 70, 140, 185, 230, 270, and 300°C. H<sub>2</sub>S was oxidized to elemental sulfur, partially in the paramagnetic form (sulfur chain radicals:  $\cdot S_x \cdot$ ,  $HS_x \cdot$ ), SO<sub>2</sub>, also partially in the paramagnetic form (SO<sub>2</sub>·<sup>-</sup>), and water. H<sub>2</sub>S<sub>n</sub> and H<sub>2</sub>SO<sub>3</sub> are also present in the reaction products. As reaction intermediates, we identified SO<sub>3</sub>·<sup>-</sup>, O<sub>2</sub>·<sup>-</sup>, and H<sub>2</sub>S<sub>2</sub>·<sup>-</sup>. The details of various identifications are given below.

The ultraviolet spectra of all the samples of the NaX zeolite used as catalysts in  $H_2S$ oxidation reaction were subsequently measured. The spectra of these samples used in reactions carried out at an O<sub>2</sub>:H<sub>2</sub>S ratio equal to 7.5:1 in the temperature range 0-300°C, showed strong absorbance in the 200- to 400-nm region (Fig. 2a). Comparing these spectra with the spectra obtained by Feher and Munzer (12) and utilizing the results of the Hückel calculations of Meyer and Spitzer (12), we attribute this absorbance to the  $H_2S_n$ -type species. Only the sample used in the reaction conducted at 185°C at an O<sub>2</sub>: H<sub>2</sub>S ratio equal to 1:1 had a spectrum with a distinct peak with a maximum at  $\sim 315$  nm (Fig. 2b). This peak was attributed to sulfur rings (12).

In Fig. 3 are plotted the amounts of  $H_2S$  removed from the flow and amounts of  $H_2S$  oxidized to  $SO_2$  (all data obtained at the stationary state) vs temperature. In the



FIG. 1. Faujasite structure influence on H<sub>2</sub>S conversion.

temperature region  $0-70^{\circ}$ C the catalytic activities of NaX and NaY zeolites at the stationary state are almost the same. At temperatures higher than  $70^{\circ}$ C the silicarich faujasite (NaY) is more active.

At 0 and 20°C, SO<sub>2</sub> was not observed in reaction products. In the temperature region 70–185°C on both NaX and NaY zeolites all H<sub>2</sub>S converted at the stationary state is oxidized to SO<sub>2</sub>.

In the temperature region 185-270 °C substantial amounts of elemental sulfur were formed. Again, at 300 °C, nearly all H<sub>2</sub>S converted is oxidized to SO<sub>2</sub>.

Investigations of the excess oxygen influence at a 70°C reaction temperature proved that the reaction rate decreases with an increase of the  $O_2:H_2S$  ratio (Fig. 4, curves a and b). At 300°C we observed a different picture. The increase in  $O_2:H_2S$ ratio causes a moderate increase in reaction rate (Fig. 4, curves c and d). On NaY, the influence of excess oxygen is much smaller at 70°C (Fig. 5).

Results of ESR investigations of the  $H_2S$  oxidation reaction conducted in a

static system are presented in Figs. 6 and 7. ESR measurements were carried out at liquid nitrogen temperature.



Fig. 2. The uv spectra of NaX samples used as catalysts in the  $H_2S + O_2$  reaction.



FIG. 3. Catalytic activity of NaX and NaY zeolites in the  $H_2S$  oxidation reaction.  $O_2: H_2S = 7.5:1$ .

After H<sub>2</sub>S adsorption on NaX at room temperature no ESR signal was observed. The spectrum shown in Fig. 6, curve a was detected immediately after admission of  $H_2S$  and  $O_2$  (ratio 1:2) to activated NaX at room temperature. This spectrum shows



FIG. 4. The influence of excess oxygen on the H<sub>2</sub>S conversion on NaX.



FIG. 5. The influence of excess oxygen on the H<sub>2</sub>S conversion of NaY.

the presence of  $S_x$  or  $HS_x$  radicals (a triplet characterized by the g factors 2.0525, 2.0325, and 2.002) (13) and small amounts of  $O_2 \cdot -$  radicals (y factors = 2.083, 2.007, and 2.002) (14). After admission at room temperature of additional oxygen up to 300 Torr and heating the sample to 150°C, no changes in signal shape and intensity were observed. Only when the sample was heated in oxygen at 230°C did the intensity of the signal of the sulfur-chain radicals substantially decrease, and a new strong signal characterized by a g factor of 2.0039 due to  $SO_3 - appeared$  (Figure 6, curve b). Subsequent evacuation of the sample and heating to 330°C for 3 hr caused the disappearance of the  $SO_3$ . signal and formation of a new signal with g factors 2.0097, 2.0054 and 2.0017 (Fig. 6, curve c). This signal is identical with the signal obtained after admission of SO<sub>2</sub> at room temperature to activated NaX zeolite and is due to the presence of  $SO_2$ . - ionradicals (8). The  $SO_2 \cdot -$  radicals generated on decationated Y zeolite have been investigated by Ono *et al.* (15). They observed two types of these radicals: One gives an ESR signal with  $g_{11} = 2.008$  and  $g_1 = 2.002$ , is unstable at temperatures greater than 300°C, and reacts with oxygen at 200°C; the other gives an ESR signal with  $g_{11} =$ 2.010 and  $g_1 = 2.002$ , is stable up to 500°C, and does not interact with oxygen. Our spectrum (Figure 6, curve c) resembles the latter, and the signal does not change after heating under vacuum at 330°C for 3 hr.

Investigating the role of  $O_2 \cdot -$  radicals in  $H_2S$  oxidation on NaX zeolite, we admitted oxygen to activated NaX samples and irradiated them with  $\gamma$  rays. In this way,  $O_2 \cdot -$  radicals were generated on the zeolite surface (16). Thirty minutes after admission of  $H_2S$  to the sample containing  $O_2 \cdot -$  at -196 °C, we observed an ESR signal with  $g_1 = 2.014$  and  $g_{11} = 2.002$  (Fig. 7). This signal, attributed to  $H_2S_2 \cdot -$  ionradicals, is nearly identical with the signal described by Lin and Lunsford (17). They obtained it after admission of  $H_2S$  to MgO irradiated in hydrogen.



FIG. 6. ESR spectra of the radial intermediates of  $H_2S$  oxidation reaction on NaX. (a)  $H_2S$  and  $O_2$ (1:2) admitted at room temperature; (b) additional  $O_2$  admitted, heating up to 230°C; (c) sample evacuated, heated at 330°C.

## DISCUSSION

In the first stage of  $H_2S$  oxidation on sodium faujasites before reaching stationary state the zeolite is acting simultaneously as an adsorbent and catalyst. When the stationary state is reached, physical adsorption no longer contributes to the removal of  $H_2S$  from the flow, and the percentage of  $H_2S$  removed is equivalent to the percentage of  $H_2S$  converted.

Sodium faujasites show a specific catalytic activity for the oxidation of H<sub>2</sub>S particularly at lower temperatures. At temperatures higher than 250°C the reaction proceeds very easily, and the influence of the faujasite structure is diminished. This is illustrated in Fig. 1. At the reaction temperature of 70°C there is a very distinct difference between the catalytic activity of NaX zeolite and the activity of the collapsed NaX. On sodium silicaalumina such as this, there is no H<sub>2</sub>S conversion at 70°C (Fig. 1, curve b). The small amounts of H<sub>2</sub>S removed from the flow during the first 6 hr are merely adsorbed. At 300°C the amounts of H<sub>2</sub>S oxidized are practically the same on both catalysts.

In the 0–70°C temperature region the main products of the H<sub>2</sub>S oxidation on sodium faujasites are elemental sulfur, water, and (at temperatures higher than 20°C) SO<sub>2</sub>. Nearly all S<sub>e1</sub> and substantial amounts of water remain in the zeolite cavities blocking centers active in this reaction. This may be the explanation for the observed equal catalytic activity of NaX and NaY in this temperature region.

At higher temperatures the reaction products are partially or fully removed from the zeolite cavities and then NaY is distinctly more active (Fig. 3). In the 70–185°C region the desorption of sulfur from zeolite cavities is still slow. Therefore most of the elemental sulfur which originated on the zeolite surface as the primary product of  $H_2S$  oxidation is subsequently catalytically oxidized to  $SO_2$ .

In the region  $185-270^{\circ}$ C sulfur leaves the zeolite surface quite rapidly, and at this temperature the noncatalytic oxidation of sulfur had not yet occurred. Therefore in the reaction products we observed both elemental sulfur and SO<sub>2</sub>.

At 300°C sulfur is oxidized catalytically (on the zeolite surface) and noncatalytically (in the reactor volume) to  $SO_2$ . Therefore  $SO_2$  predominates again in the reaction products. Steijns *et al.* (10) observed  $SO_2$ in the reaction products only a temperatures higher than 200°C. They postulated that



Fig. 7. The ESR spectrum obtained after admission of  $H_2S$  at -196 °C to NaX zeolite irradiated in presence of  $O_2$ .

in the temperature region 100–200°C the formation rate of SO<sub>2</sub> is at least a factor 100 smaller than the oxidation rate of  $H_2S$ . We observed substantial amounts of SO<sub>2</sub> even at 70°C, and in the region 100-200°C  $SO_2$  was the main reaction product. The formation of SO<sub>2</sub> and H<sub>2</sub>S conversion depend strongly on reaction conditions. In the experiments summarized in Fig. 3 we used a large excess of oxygen (O<sub>2</sub>:H<sub>2</sub>S =7.5:1) and a relatively long contact time. When we used a contact time approximately five times shorter (a 200-ml/min gas flow and the same amounts of H<sub>2</sub>S and  $O_2$  as previously), the  $H_2S$  conversion on NaX at 70°C was distinctly higher than the H<sub>2</sub>S conversion on NaY at 185°C.

The differences in catalytic activity between NaX and NaY zeolites, i.e., zeolites which have the same structure and differ only in Si/Al ratio and in amounts of Na<sup>+</sup> cations per unit cell, can be explained in terms of different types of  $H_2S$  chemisorption. Karge and Rasco (18) used ir spectroscopy for investigations of  $H_2S$ chemisorption on faujasite-type zeolites. They found that on the alumina-rich faujasites (type X) heterolytic dissociative chemisorption occurs:

$$H_2S_{ads} \rightarrow HS^- + H^+,$$

 $H^+$  forming a surface hydroxyl with the lattice oxygen. The amount of  $H_2S$  dissociated in this manner decreases with increasing Si/Al ratio, and on NaY the bands due to formation of  $HS^-$  and surface hydroxyls were not observed.

Imai and Habgood (14) observed, after  $H_2S$  adsorption at room temperature on silica-rich faujasite-type zeolite (NaY) activated and treated with  $H_2$ , an ESR spectrum which showed on orthorhombic g-tensor and which had hyperfine splitting due to an H atom. Consequently, we presume that on NaY another type of dissociative chemisorption may occur:

# $H_2S_{ads} \rightarrow HS \cdot + H \cdot$

Conducting the  $H_2S$  oxidation reaction on NaX at 70°C, we observed a rather unusual effect. The high excess of oxygen distinctly lowered the reaction rate. The

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excess of oxygen influence is not clear yet. Probably it lowers the concentration of the active radical-type reaction intermediates and increases the amount of species (e.g.,  $SO_3^{-}$ ) blocking surface active centers. On NaY zeolite the negative influence of excess oxygen is not so distinct (Fig. 5).

During the initial stage of  $H_2S + O_2$ reaction  $H_2S$  is oxidized to elemental sulfur. We did not observe  $SO_2$  in the reaction products for a long time from the beginning of the reaction at  $O_2: H_2S = 1:1$  (at 70°C, for 240 min; at 185°C, for 60 min) (8). Karge and Rasco (18) did not observe  $SO_2$ in ir spectra after adsorption of  $H_2S$  and  $O_2$  on NaX zeolite and heating the sample up to 400°C. On the basis of kinetic studies Steijns *et al.* (11) concluded that the primary reaction product is sulfur.

All the results discussed above suggest that on sodium faujasites  $H_2S$  is oxidized first to elemental sulfur and subsequently sulfur is oxidized to SO<sub>2</sub>. On these catalysts the  $H_2S$  oxidation proceeds in a different way than was postulated for bauxite-type catalysts (1), i.e.,  $H_2S$  oxidation to SO<sub>2</sub> and formation of elemental sulfur in the Claus reaction ( $H_2S + SO_2$ ).

Sulfur dioxide formed in faujasite cavities from the oxidation of elemental sulfur is chemisorbed with the formation of an SO<sub>3</sub> complex (one oxygen of this complex belongs to the zeolite lattice), and after electron addition the ion-radical SO<sub>3</sub>. – is formed (Fig. 6, curve b). The nature of the electron-donor centers is still not clear. They may be Fe<sup>2+</sup> impurities, lattice defects, or anion-type reaction intermediates. The strong signal of SO<sub>2</sub>. – obtained after adsorption of SO<sub>2</sub> on NaX even at room temperature (8) indicates that at the faujasite surface electrons are available.

Steijns et al. (11) postulate an oxidationreduction mechanism for the oxidation reaction of  $H_2S$  on NaX zeolite. In this proposed mechanism there is first the oxidation step:

$$\cdot$$
S - (S)<sub>x-2</sub> - S· + O<sub>2</sub>  $\rightarrow$  [S<sub>x</sub>O<sub>2</sub>]

The second step in the mechanism is the reduction of  $[S_xO_2]$  with H<sub>2</sub>S yielding sulfur and water (the equation was not written). This mechanism is based mainly on two observations:

(i) Sulfur chain radicals were detected in the ESR spectra of activated NaX zeolite after admission of  $H_2S$  at 150°C in N<sub>2</sub> flow. But, as Steijns *et al.* mention, the activation procedure used may still allow some oxygen species to exist on the zeolite surface. Other authors (18, 20), and we ourselves, did not detect the elemental sulfur after  $H_2S$  adsorption on sodium faujasites in the complete absence of oxygen at temperatures up to 300°C.

(ii) Steijns et al. observed that after admission of a nitrogen-oxygen mixture at 150°C to a NaX zeolite containing sulfur, the intensity of the paramagnetic sulfur signal (g = 2.028) became smaller by a factor of 20. Two minor signals appeared which were attributed to  $S_x O_2 \cdot (g = 2.005)$ and  $S_xO^{-}$  (g = 2.013). A signal with g = 2.005 was observed also after admission of SO<sub>2</sub> to NaX zeolite. It is our opinion, however, that the generation of  $S_xO_2$ . radicals after  $SO_2$  sorption is not very probable. ESR investigations of SO<sub>2</sub> adsorption on faujasite-type zeolites (8, 15)proved that in this process  $SO_2 \cdot \overline{\phantom{a}}$  ionradicals are formed. We presume that the mechanism of H<sub>2</sub>S oxidation with molecular oxygen on NaX, especially at the initial stage of the reaction, is more complicated. At the beginning of the reaction there is no elemental sulfur present on the zeolite surface. The reaction has to start from the interaction between adsorbed reactants. As was mentioned before (18, 20), on NaX zeolite, the H<sub>2</sub>S is chemisorbed dissociatively:

$$H_2S_{ads} \rightarrow HS^- + H^+,$$
 (1)

and the proton will form a hydroxyl with the lattice oxygen. Oxygen is adsorbed on Na<sup>+</sup> cations and it was found that  $O_2$  molecules so adsorbed trap electrons very efficiently, giving rise to an ESR signal characteristic of the superoxide ion  $O_2 \cdot -$ (14, 19). Therefore if the Na<sup>+</sup> O-O electron trap and HS<sup>-</sup> are in close proximity, the following reaction may occur:

$$\begin{aligned} \mathrm{HS}^{-} + \mathrm{O}_{2\mathrm{ads}}(\mathrm{Na}^{+}) &\rightarrow \\ \mathrm{HS} \cdot + \mathrm{O}_{2} \cdot^{-}(\mathrm{Na}^{+}). \end{aligned} (2)$$

Takahashi (21) suggested that the most probable reaction of HS·radicals is:

$$2HS \cdot \to H_2S + \cdot S \cdot. \tag{3}$$

Also very probable are two other reactions of  $HS \cdot :$ 

$$2\mathrm{HS} \cdot \to \mathrm{HSSH} \tag{4}$$

$$\mathrm{HS}\cdot + \mathrm{HS}^{-} \to \mathrm{H}_{2}\mathrm{S}_{2}\cdot^{-} \tag{5}$$

Both intermediates were observed by us,  $H_2S_2$  by uv spectra and  $H_2S_2$ .<sup>-</sup> by ESR spectra (Figs. 2 and 7).  $H_2S_2$ .<sup>-</sup> ought to react with oxygen:

$$\mathrm{H}_{2}\mathrm{S}_{2}\cdot^{-} + \mathrm{O}_{2} \to \mathrm{H}_{2}\mathrm{S}_{2} + \mathrm{O}_{2}\cdot^{-}.$$
 (6)

We observed all these reaction intermediates except  $HS \cdot .$  The difficulties with  $HS \cdot$  indentification are probably connected with some similarity of this spectrum with the spectrum of sulfur chain radicals  $(HS_x \cdot \text{ or } \cdot S_x \cdot)$ . This latter signal is one or a few orders of magnitude stronger during the  $H_2S$  oxidation reaction.

The reaction steps leading to formation of water are still only hypothetical. One possible way is the reaction between  $O_2 \cdot \overline{\phantom{a}}$ and physically adsorbed  $H_2S$ :

$$H_2S_{ads} + O_2 \cdot \overline{\phantom{a}} \rightarrow HS \cdot + HOO^-$$
. (7)

This reaction step is very probable. Lunsford (22) reported that the  $O_2 \cdot \overline{}$  radical easily takes a hydrogen atom from olefin molecules. The C-H bond energy in olefins ( $\simeq 359$  kJ/mol) is higher than the energy of the H-S bond in H<sub>2</sub>S ( $\simeq 343$ kJ/mol). Even more probable is the reaction:

$$H_2S_2 + O_2 \cdot \overline{\phantom{a}} \rightarrow HSS \cdot + HOO^-$$
. (8)

The HOO- ions may react with H+

supplied by surface hydroxyls [Eq. (1)]:

$$\mathrm{HOO}^{-} + \mathrm{H}^{+} \rightarrow \mathrm{H}_{2}\mathrm{O}_{2}. \tag{9}$$

Samples of NaX and NaY, fresh and after 12 hr reaction time, have been tested for acidity using a titration method. We did not observe any appreciable changes in sample acidity before and after the  $H_2S$ oxidation reaction. Therefore some reaction step involving proton addition is obvious. The  $H_2O_2$  will easily decompose

$$H_2O_2 \to H_2O + O, \qquad (10)$$

and atomic oxygen will oxidize next the  $H_2S$  molecule.

The H<sub>2</sub>S oxidation reaction on NaY will start differently. Probably the HS  $\cdot$  radicals are formed after H<sub>2</sub>S adsorption.

The considerable number of radicals, ionradicals, and ions identified so far as intermediates in the  $H_2S$  oxidation reaction on sodium faujasites indicates that the mechanism of this reaction is rather complicated. Additional investigations involving ESR, ir, and uv measurements are necessary to elaborate the complete reaction mechanism.

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